



Faecal Sludge Treatment and Reuse in Emergencies: A Case Study from Mahalaxmi Municipality, Nepal

Presenting Authors

Reetu Rajbhandari

Bipin Dangol

Rajendra Shrestha

Environment and Public Health Organization (ENPHO)



Partner organizations

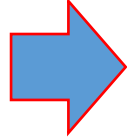


- Background
- Flow Diagram with capacity of each component
- Present Status
- Laboratory Analysis Report
- Performance of Treatment Plant
- Lesson Learnt
- Challenges
- Way Forward

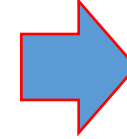




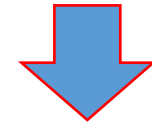
Devastating earthquake in April 2015 in Nepal



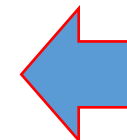
People residing in campsites



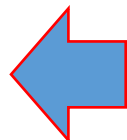
Construction of temporary toilets in campsites



Overflowing toilets in campsites



Construction of treatment plant



Faecal sludge reuse complex



OSTASIATISCHER VEREIN BREMEN E.V.
GEGR. 17. JANUAR 1901



Financial support



Land area (300m²) provided by:
Saligram Orphanage



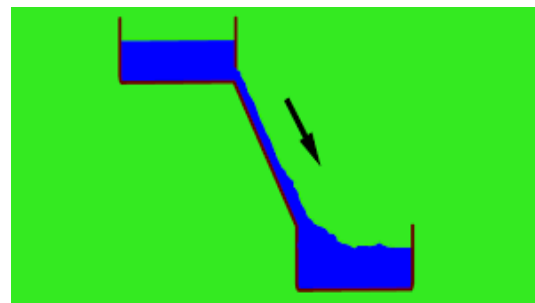
Technical support: ENPHO and CDD Society



Construction Cost and Prefabricated Component's Cost = USD 70,600



Designed treatment capacity 6 m³/week

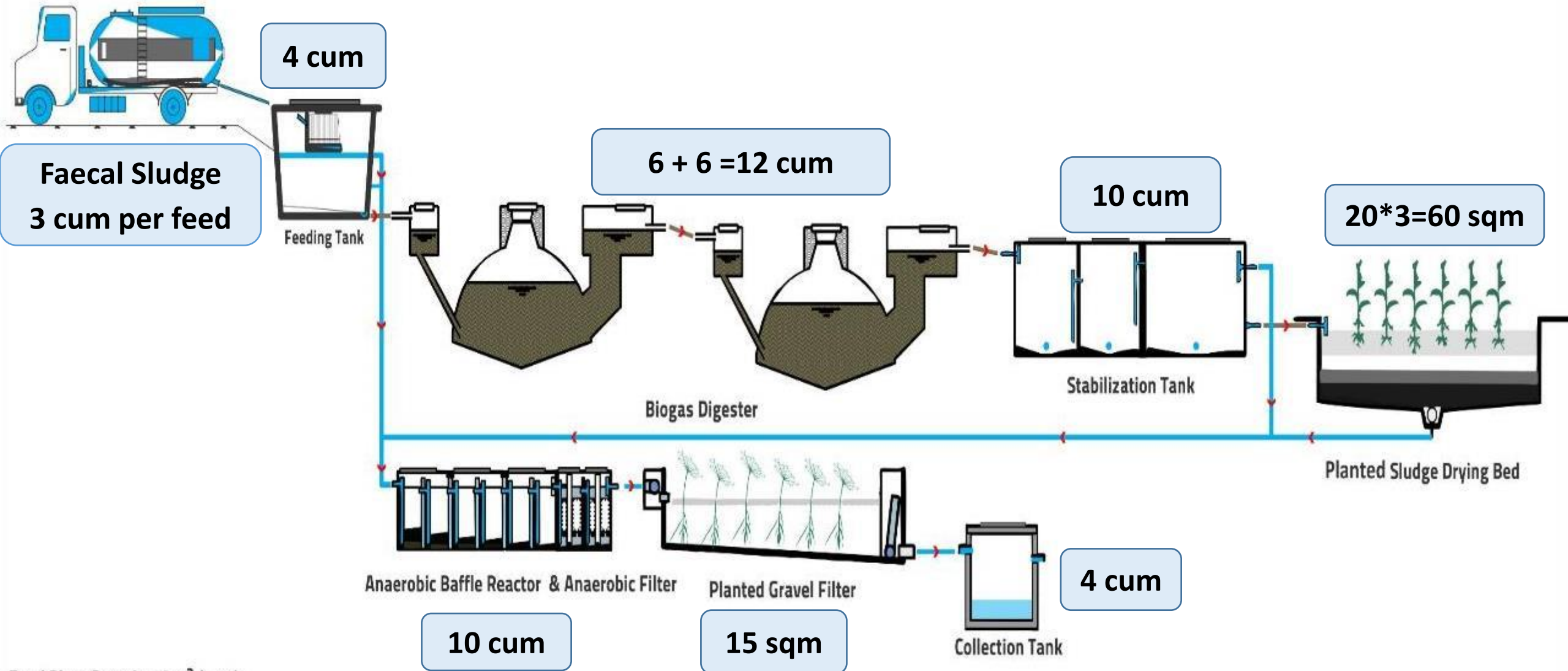


Gravity based system



No skilled labor required for day to day operation

Flow Diagram with Capacity of each Component



Faecal Sludge
3 cum per feed

4 cum

6 + 6 = 12 cum

10 cum

20*3=60 sqm

4 cum

10 cum

15 sqm

Present Status (327 days of operation)



Number of loads arrived : **80**



Volume of Biogas used: **196 m³**



Volume of treated water generation: **4m³/week**



Number of sampling done: **3 times**

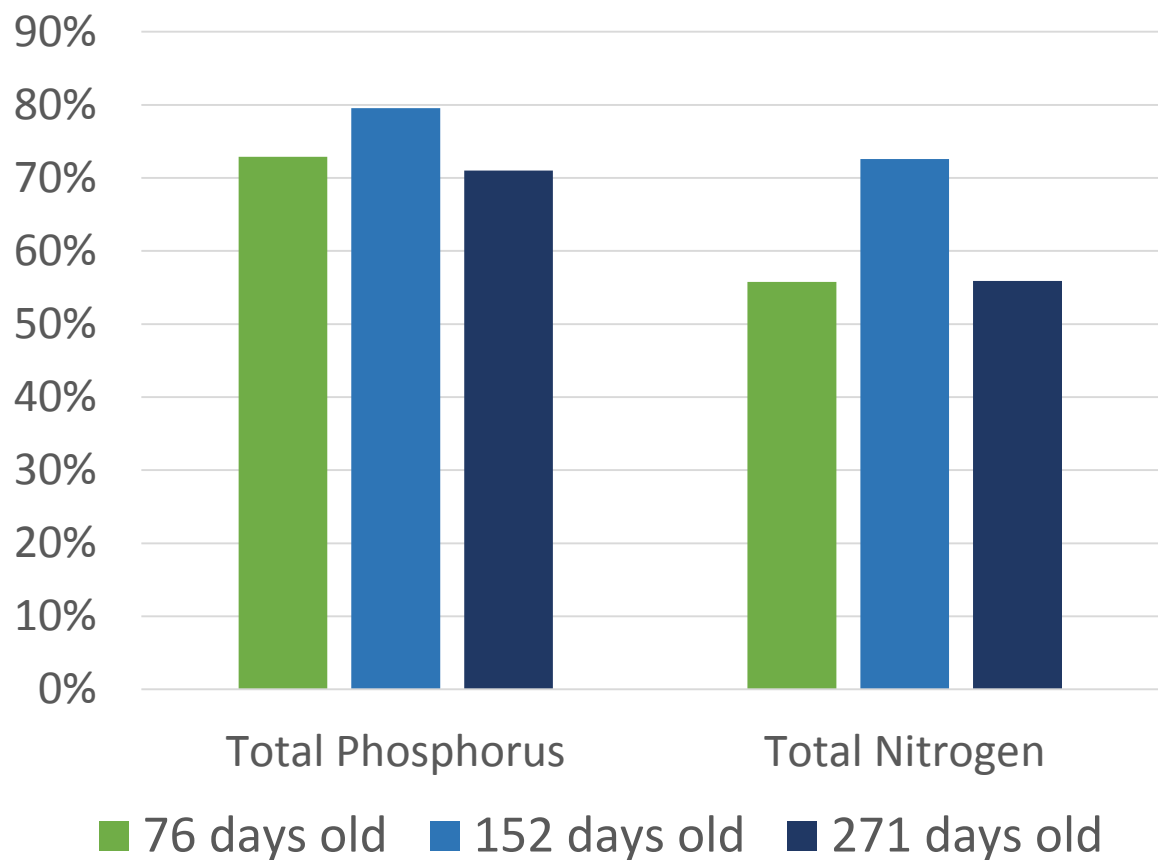


Laboratory Analysis Result

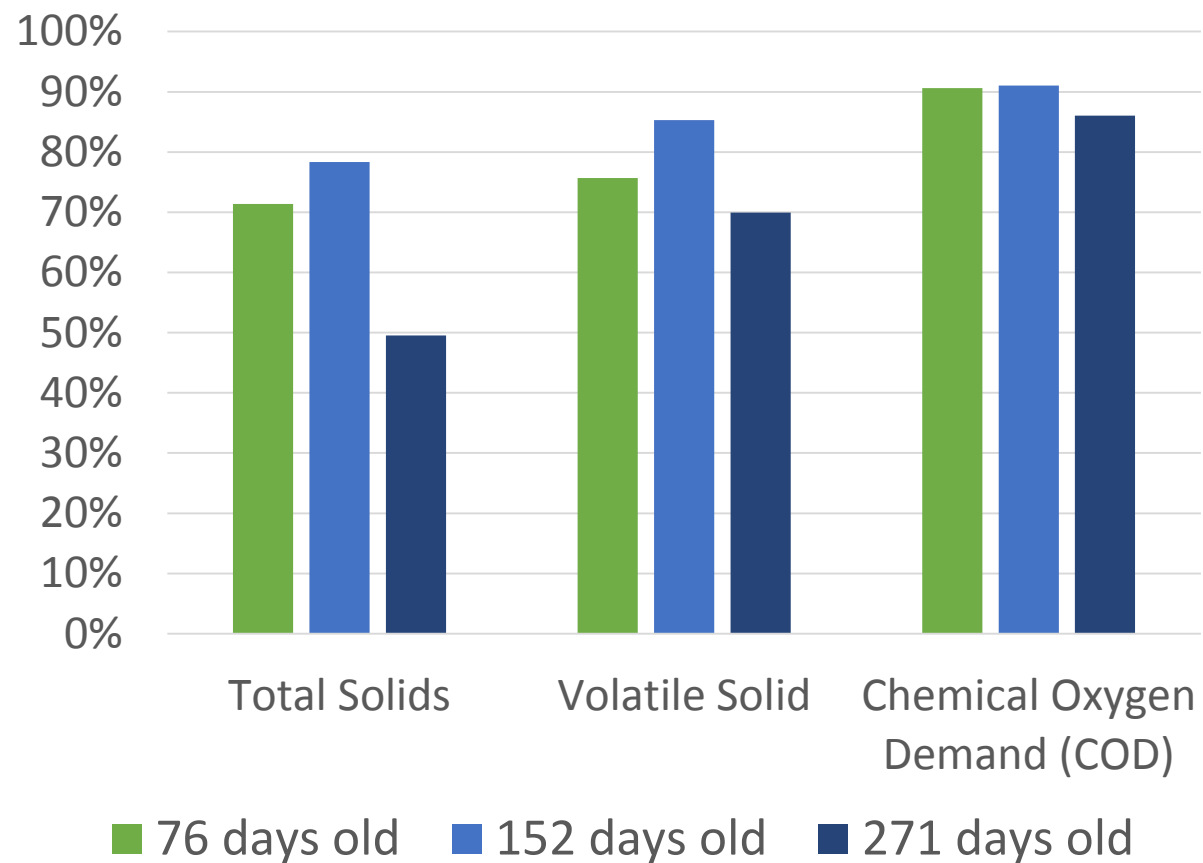


Parameters	Unit	After 76 days of operation			After 152 days of operation			After 271 days of operation		
		Pre- Monsoon			Monsoon			Post-Monsoon		
		FT	PGF outlet	Removal (%)	FT	PGF outlet	Removal (%)	FT	PGF outlet	Removal (%)
pH	-	7.9	8.1	NA	7.3	7.5	NA	7.5	8	NA
Electrical conductivity	µS/cm	11840	5280	55.41%	8370	2590	69.06%	5620	4410	21.53%
Total Solids	mg/L	5554	1590	71.37%	4911	1064	78.33%	4997	2522	49.53%
Volatile Solids	mg/L	2206	536	75.70%	2172	319	85.31%	2154	648	69.92%
Total Alkanity as CaCO3	mg/L	4390	2615	40.43%	3730	319	91.45%	3040	2240	26.32%
Nitrogen-Ammonia	mg/L	1240	572	53.87%	896	264	70.54%	770	450	41.56%
Nitrate	mg/L	0	0	NA	5.2	0.5	90.38%	4.9	ND(<0.2)	96.00%
Total Phosphorus	mg/L	107	29	72.90%	93	19	79.57%	30	8.7	71.00%
Total Nitrogen	mg/L	1384	612	55.78%	1003	275	72.58%	1370	604	55.91%
Total Kjeldahl Nitrogen (TKN)	mg/L	1384	612	55.78%	1002	274	72.65%	1369	604	55.88%
Organic Dry Matter	mg/L	2206	536	75.70%	2172	319	85.31%	2154	648	69.92%
Chemical Oxygen Demand (COD)	mg/L	5244	492	90.62%	3120	280	91.03%	5563	775	86.07%
Potassium (K)	mg/L	299	200	33.11%	407	141	65.36%	113	190	-68.14%
Helminths	Present/Absent	Absent	Absent	-	Absent	Absent	-	Present	Absent	-
E.coli	CFU/mL	TNTC	TNTC	-	TNTC	TNTC	-	TNTC	TNTC	-
*FT= Feeding Tank		*CFU= Colony Forming Unit					*NA= Not Applicable			
*PGF= Planted Gravel Filter		*TNTC=Too Numerous To Count					*ND= Not Detected			

Nutrient Removal Efficiency of the Treatment Plant



Solids and Organic Removal Efficiency of the Treatment Plant



- High septic tank emptying demand
- Limited design capacity of treatment plant
- Social acceptance
- Low awareness in FS workers (desludging service providers) on health safety



- Need-based placement
 - Community support
 - Political support
 - Private operator's support (honey sucker's role)
 - Optimum use of end-products

- Minimize and simplify operational works



Desludging Vehicle



Caretaker of FSTP

- Continue on-job training on O&M
- Business plan for sustainability
- Handover of FSTP to local NGO by March, 2018
- Monitoring and research
- Evidence-based advocacy on FSM
- Explore possible replication of the system





Inauguration by Chief District Officer



Visitors - Government Officials



Thank you for your attention!