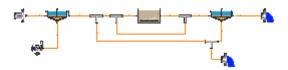
RESOURCE RECOVERY FROM FECAL SLUDGE AN ELEMENTAL APPROACH

Kartik Chandran

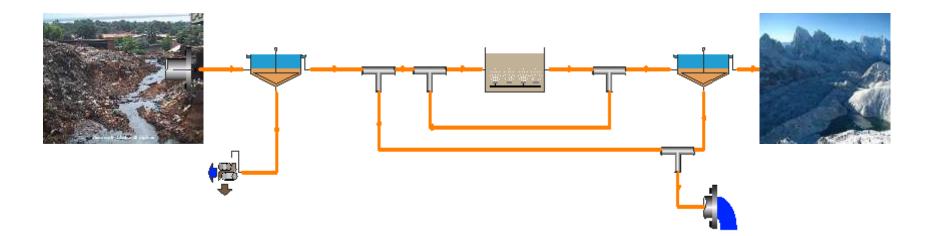
Columbia University

Fecal Sludge management Conference, Durban, October 30th, 2012



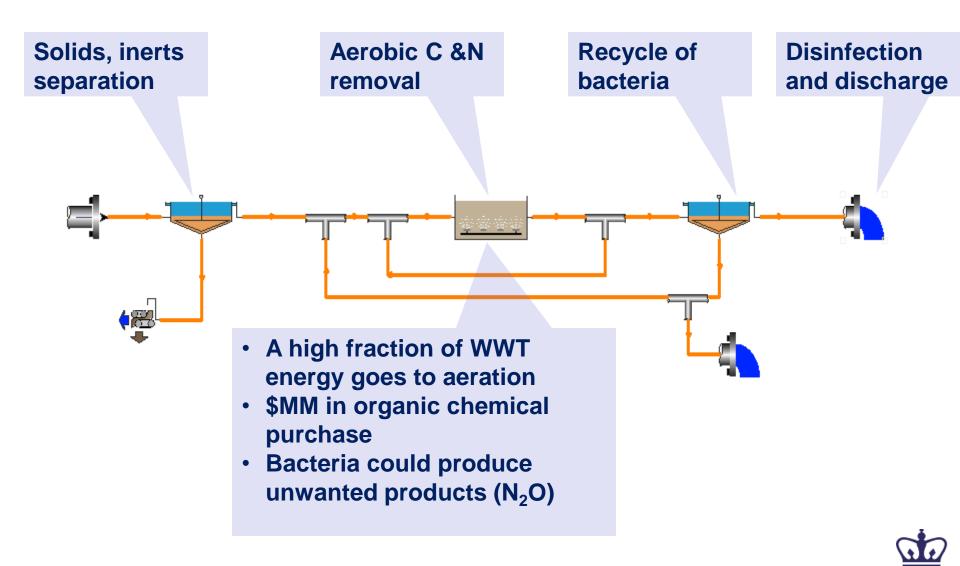




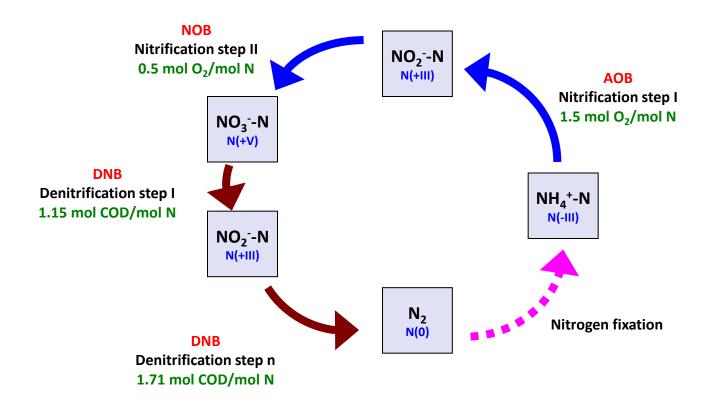




Brief overview of biological treatment

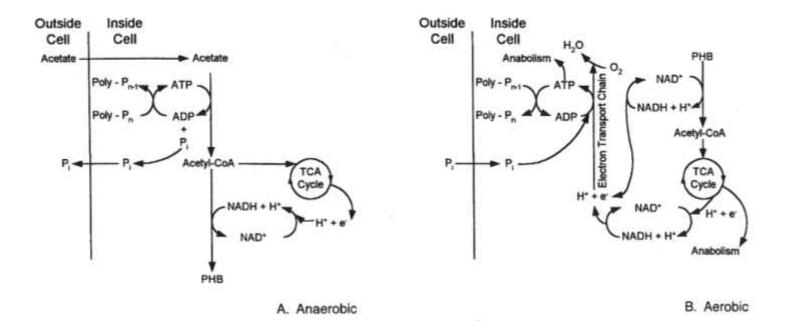


Biological N-removal





Biological phosphorous removal



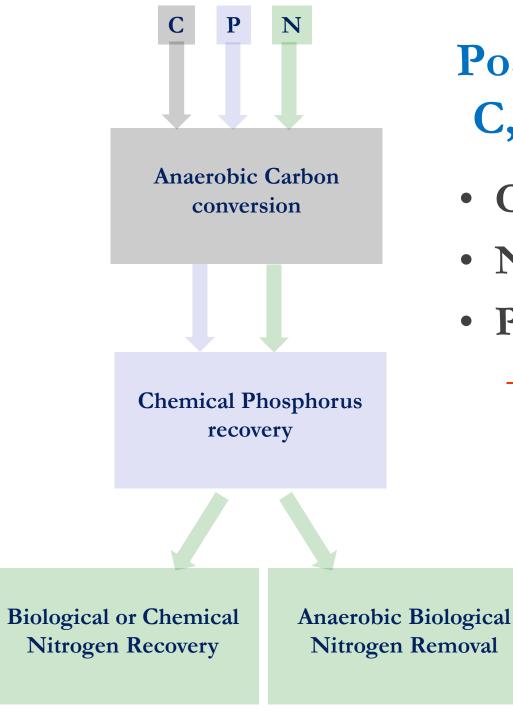


Mass loading of organics and nutrients entering 14 NYC WWTPs

- Flow: 1.2 billion gallons per day
 - 1860 tons of organic carbon per day
 - 280 tons of N(-III) per day
 - 60 tons of P(+V) per day







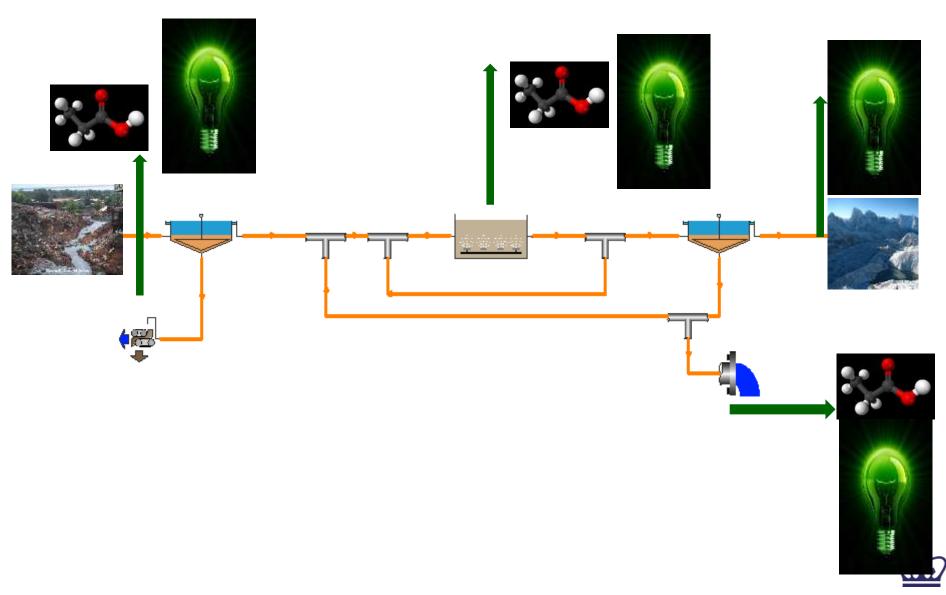
Possible flowsheet for C, N and P recovery

- C-reduction
- N-no redox cycling
- P- no redox cycling

 How to monetize recovery of energy or chemical resources with environmental process objectives



Engineered Resource Recovery from 'Waste' Streams

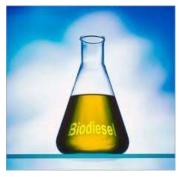


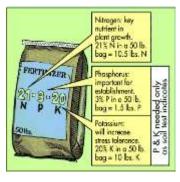


Conversion of fecal sludge into biodiesel







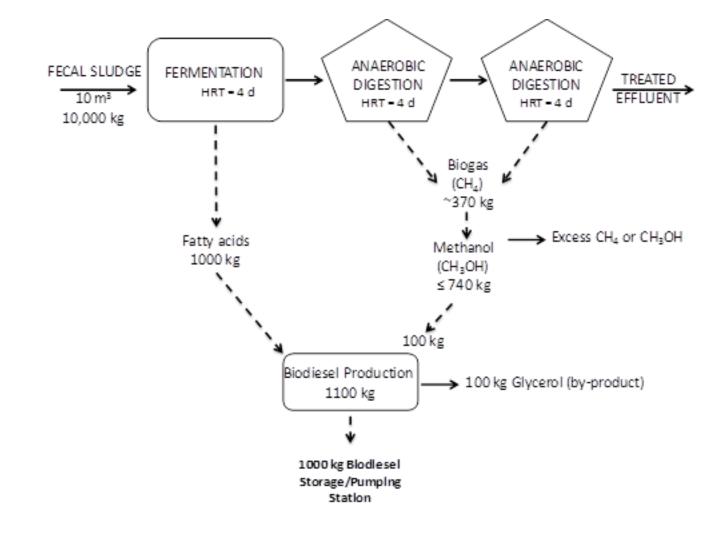








Faecal Sludge to Biodiesel Process Schematic





Piloting in Kumasi, Ghana



- Entirely surrounded by FS lagoons and landfill
- Facility completely off-grid
 - No municipal water, or power available on site



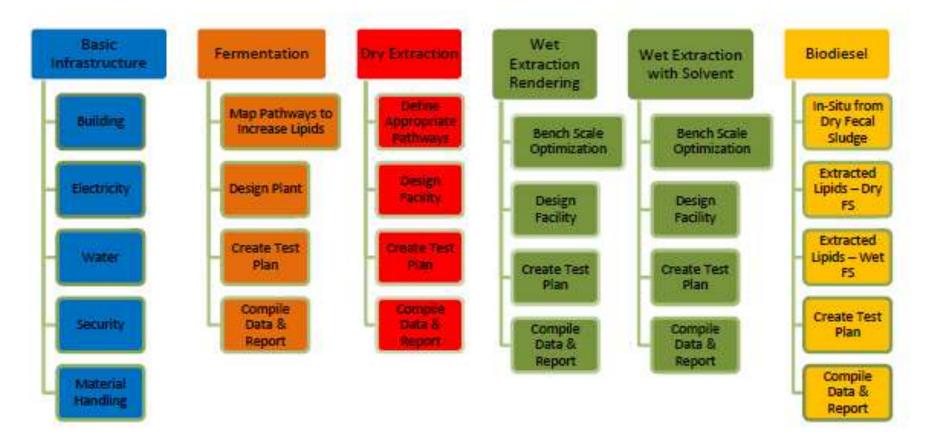
Piloting in Kumasi, Ghana



- Q=10,000L/d
- HRT = 12d
- Feedstock fecal sludge
- End products methane, chemicals, biodiesel



FS2BD Project Map





Brief process calculations

| Parameter | Value |
|------------------------|------------------|
| Process design flow | 10,000 L/d |
| Inherent lipid content | 50 kg/d |
| Biodiesel potential | 57 L/d biodiesel |

| Parameter | Value |
|------------------|--|
| Methane produced | 45 m ³ /d, assuming 0.3 m ³ / kg COD removed and 50% COD removed |
| N-recovered | 20 kg/d, assuming 2000 mg NH_3/L in FS |
| P-recovered | 2.75 kg/d, assuming 275 mg P/L in FS |



Fecal sludge to biodiesel

- Construction complete
- Processing of FS and conversion
 experiments ongoing
- Developing lab and testing facilities onsite





Opportunities for increasing process efficiency



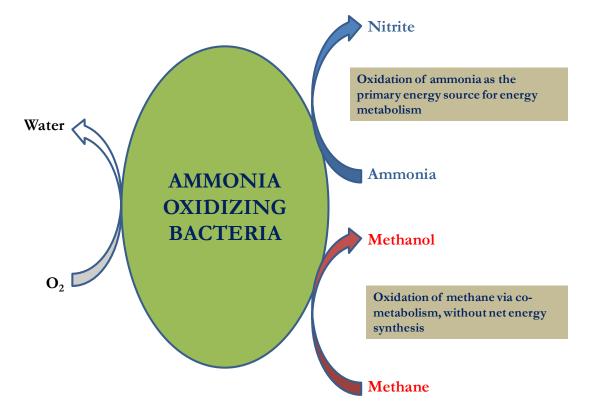
Internally producing lipids

| Parameter | Value |
|------------------------|---|
| Process design flow | 10,000 L/d |
| Inherent lipid content | 50 kg/d |
| SC-VFA yield expected | 60 kg COD/d Assuming: 20 g COD/L in the influent FS Assuming: 30% VFA COD/FS COD by fermentation |
| Lipids produced | 1067 – 6933 g lipids/d |
| Total lipids | 51067 -56933 g/d |
| Biodiesel potential | 58 – 65 L/d biodiesel |

• Also vastly opens up the choice of substrate feedstocks



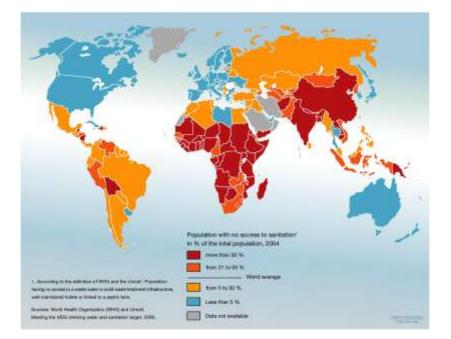
Chemical Recovery Methane to bio-methanol



- Concomitant oxidation of CH₄ and CO₂ fixation
- Prospect of combining C &N cycles



Resource recovery is not the panacea



| Food security | Food security | Food security |
|-------------------------------|-------------------------------|-------------------------------|
| Technology and engineering | Technology and engineering | Technology and engineering |
| Recover C-energy | Recover C-energy | Recover C-energy |
| Recover P | Recover P | Recover P |
| Recover N | Recover N | Recover N |



Contact information

Kartik Chandran Associate Professor Director, Wastewater and Climate Change Program Director, Columbia University Biomolecular Environmental Sciences Email: kc2288@columbia.edu Phone: (212) 854 9027 URL: www.columbia.edu/~kc2288/



Acknowledgements

The Bill & Melinda Gates foundation Fecal Sludge to Biodiesel project team



Alternate feedstocks and endpoints

- Waste cooking oil
 - Evaluate biodiesel yield and quality after multiple use
 - Follows direct biodiesel pathway
- Any organic stream, literally
 Follows fermentation pathway
- Bio-butanol possible with high carbohydrate wastes



Are there other benefits?

Environ. Sci. Technol 2010, 44 4585-4511

N₂O Emissions from Activated Sludge Processes, 2008–2009: Results of a National Monitoring Survey in the United States

IGON HO AHN,[†] SUNGPYO EIM,^{†,*} HONGKEUN PARE,[†] BRIAN RAHM,[†] ERISHNA PAGILLA,[†] AND EARTIE CHANDEAN^{*,†}

Department of Earth and Environmental Ingéniering Columbia University, New York, New York 10007, and Department of Civil, Architectural and Environmental Engineering, Mitsois Institute of Technology, Chicago, B. neered BNR facilities, while effective to varying degrees in reducing aqueous nitrogen pollution could emit up to 7% of the influent retrogen load as generate nitrous could (N₂C) and retric could (NC), as described for the nitrifying R-stage of the Dokhaven-Slaisjeschijk WWTP in The Netherlands (I). Such emissions are deleterious to the environment. The growthouse equivalence of NO is about three hundred times that of earbein dioxide and both N₂C) and NO contribute in depletion of the course layer (2).

Although, from a fundamental perspective, N₂D and NO are known intermediates in denitrification (3, 4) and nitrifection (5–3), the not-contribution of HNR processes to NoO emissions from wastewater treatment has only recently been acknowledged (70). Based on the latest U.S. Environmental Protection Agency (USEPA) report on sources and sinks of N₂O from wastewater treatment operations, denitrification in anosic remus is implicated as the dominant source of NoO from UNIC actional Defension and the form

- N_2O is produced during both nitrification and denitrification
 - Redox cycling of N
- Poorly designed and operated ww treatment plants produce and emit higher N_2O



Ahn et al., 2010a,b, Yu et al., 2010, Yu & Chandran, 2010, Lu & Chandran, 2010, Chandran et al., 2011

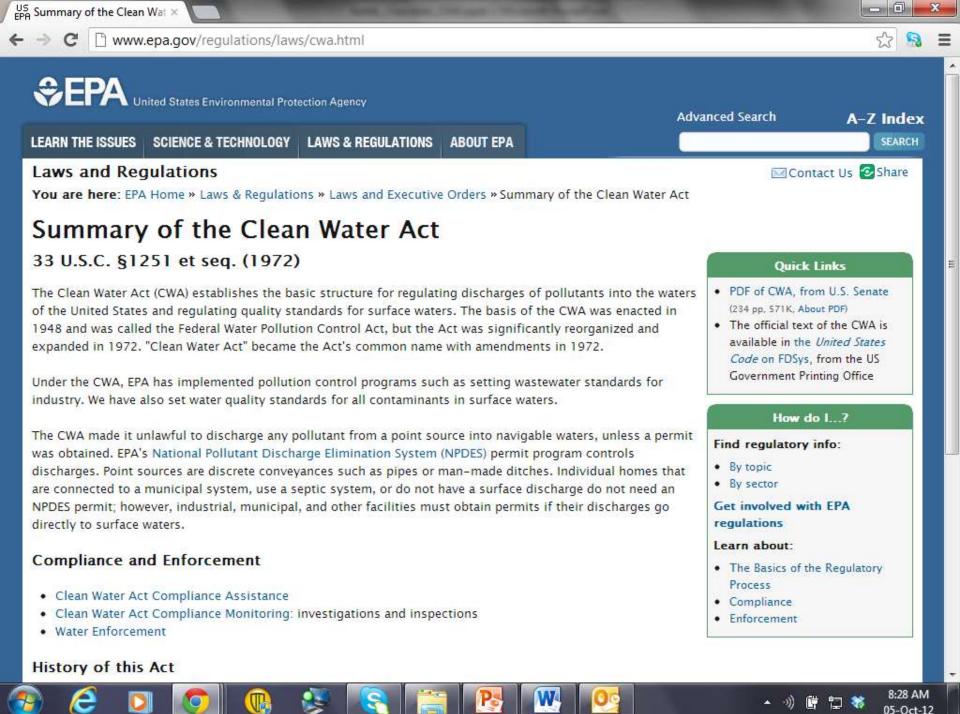
Resource recovery - Sometimes low tech is enough

Sewage sludge to biodiesel

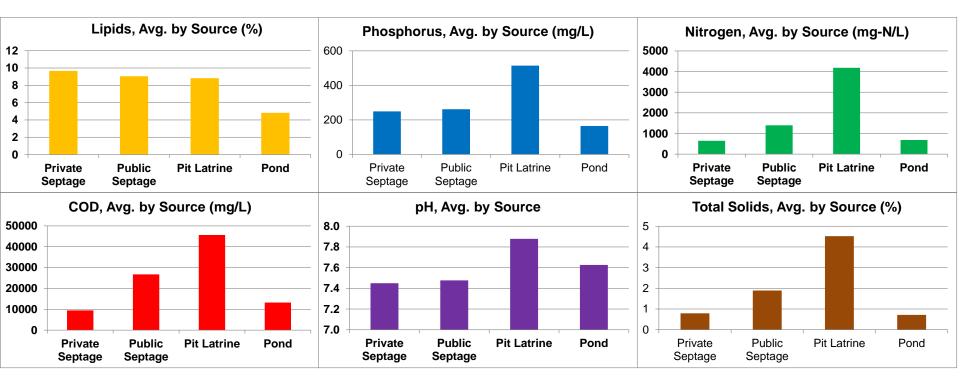


- Using the fat content of biosolids
- Using MeOH for fuel production instead of Nremoval





Characteristics of fecal sludge





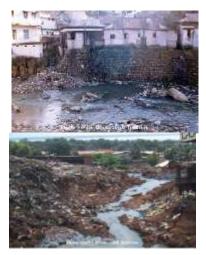


Wicked Problem, about 70% of the world's population will live in cities by 2050









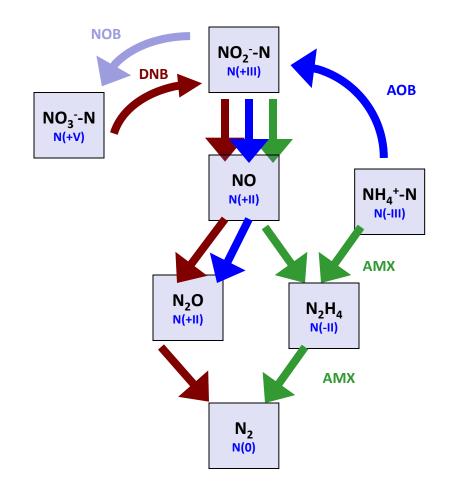












- Several intermediates reactive
 NO₂⁻-N, NO, NH₂OH
 - Control expression of pathways
- How to resolve activities?
- How to resolve contribution to mass balances?

Ahn et al., 2008, Baytshtok et al., 2008, 2009, Park et al., 2010a,b, Lu et al., 2011a,b, Lu et al, 2012

Engineered BNR systems are typified by multiple activities in concert or competition

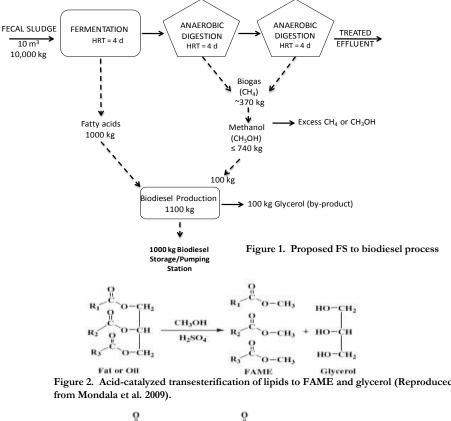
Fecal Sludge to Biodiesel

Project objectives

- 1) Develop a robust and efficient fermentation-based technology for producing biodiesel from FS.
- 2) Understand costs and potential revenue streams of fecal sludge-fed biodiesel production.
- 3) Identify and prepare for structures and procedures needed to successfully implement and operate a full-scale FS-fed biodiesel plant as a social enterprise in Ghana.

Fermentation-based technology for producing biodiesel from fecal sludge:

- 1. Fermentation of fecal sludge organics testing different biocatalysts.
- 2. *In-situ* acid catalyzed (trans)esterification of fatty acids for production of fatty acid methyl-esters.
- 3. Anaerobic digestion of residual streams.



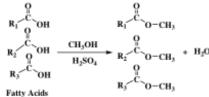
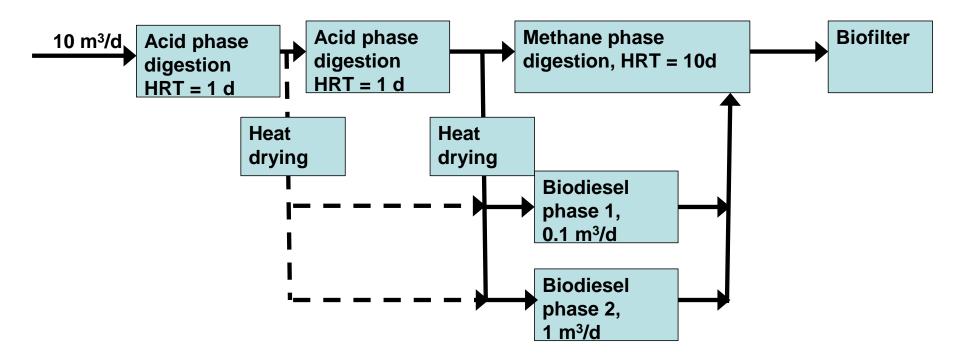


Figure 3. Acid-catalyzed esterification of fatty acids to FAME and water (Reproduced from Mondala et al. 2009).

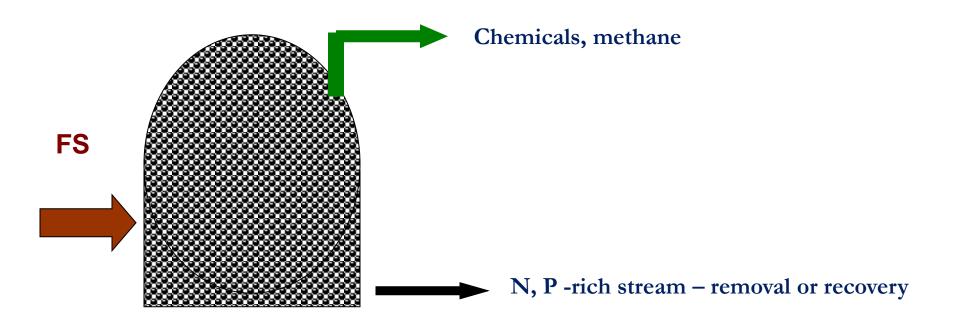
Adapted from CU Proposal Narrative and Appendix II: Sludge-fed Biodiesel Technology Landscape, 2011

Process schematic





Recovery of Carbon from FS What our industry already knows and does



Still some limitations to widespread use of digester gas for energy

Dual-Phase Digestion and Fermentation of SS



PDS fermentation and storage at 26th Ward WPCP in New York City, 2002

- Fermentation of PDS to produce VFA
 - Used mainly for denitrification
 - Kinetics higher than MeOH
- Acid-digestion of surface froth and scum
 - Reduced foaming
 - VFA recovery

