RECOVERY AND UTILIZATION OF VOLATILE FATTY ACIDS FROM ORGANIC WASTE FOR BIODIESEL PRODUCTION AND MICROBIAL INACTIVATION

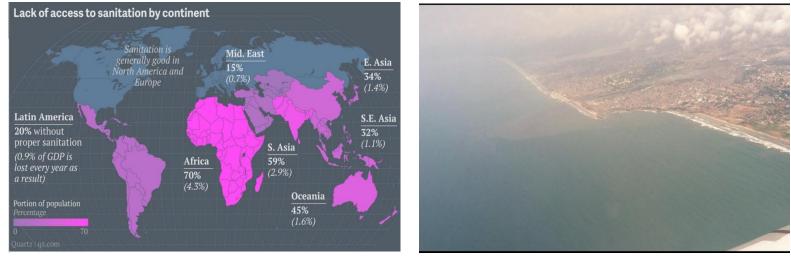
Shashwat Vajpeyi, Kartik Chandran* Columbia University

FSM3

Hanoi, Vietnam, January 21st, 2015







Lack of adequate sanitation is a global challenge



Is it possible to link sanitation with higher value chain biofuels and commodity chemicals?

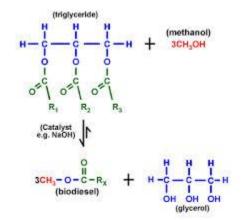
Often limited by access to reliable energy inputs and chemicals



Fecal sludge to biodiesel

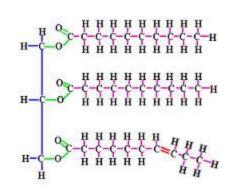
• Biodiesel





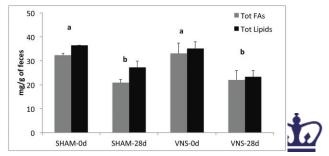
• Lipids

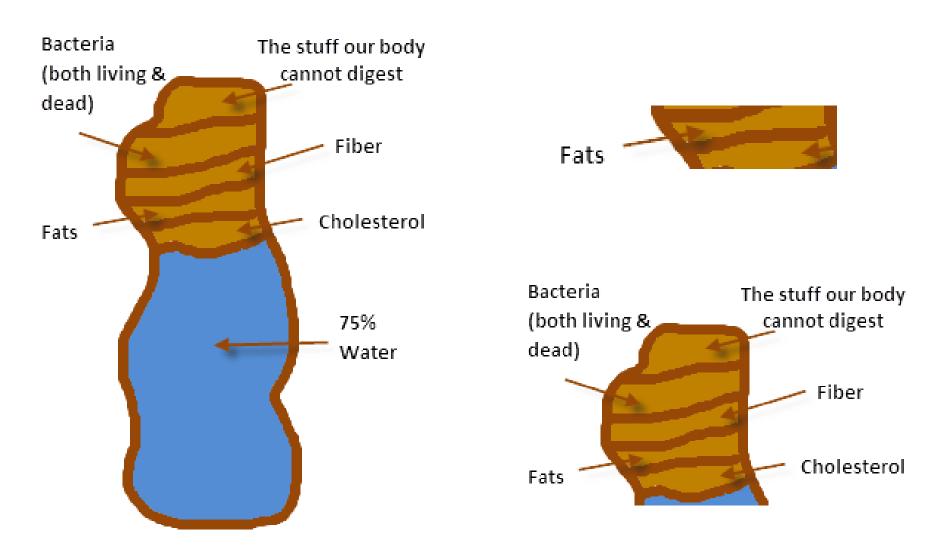




• Lipids in feces

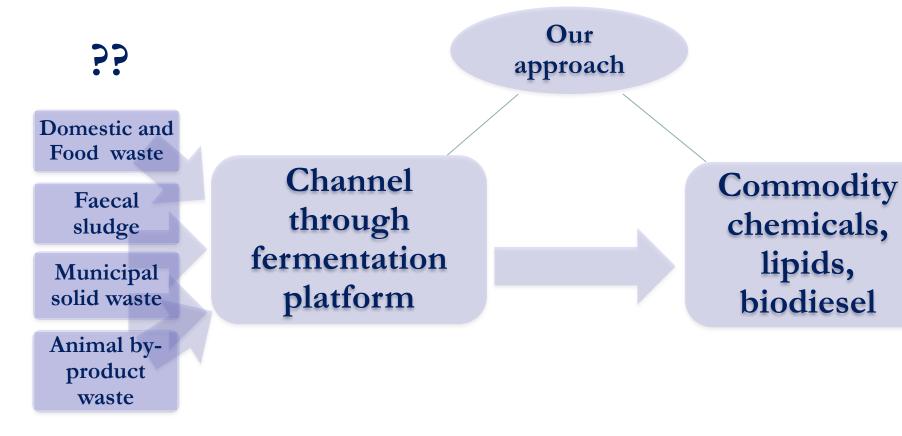






• Biodiesel process agnostic to 'waste' stream?

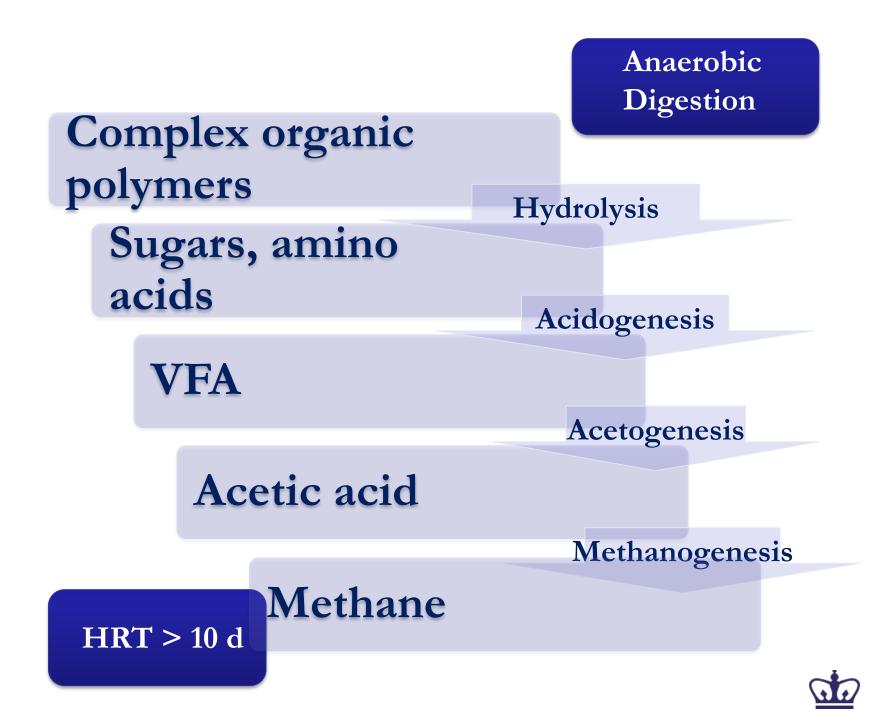


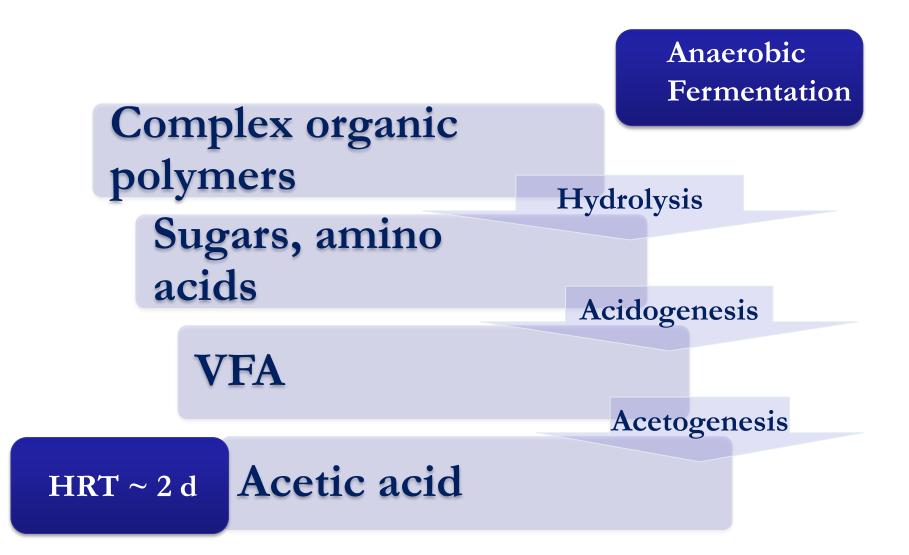


BILL& MELINDA GATES foundation









- Fermentation is more advantageous than just anaerobic digestion
- Fermentation can be incorporated into existing digestion processes



Overview of our process











Organic waste Anaerobic fermentation to produce volatile fatty acids (VFA)

Convert VFA to lipids Harvest and extract lipids Convert lipids to biodiesel

Conversion of VFA to Lipids

Different COD sources

- VFA from food waste fermentation
- Synthetic VFA
- Glucose
- Different initial VFA concentrations



Batch reactor

6:1:3 acetate, propionate, butyrate. 2 day HRT

Lipid content of *C*. *albidus*



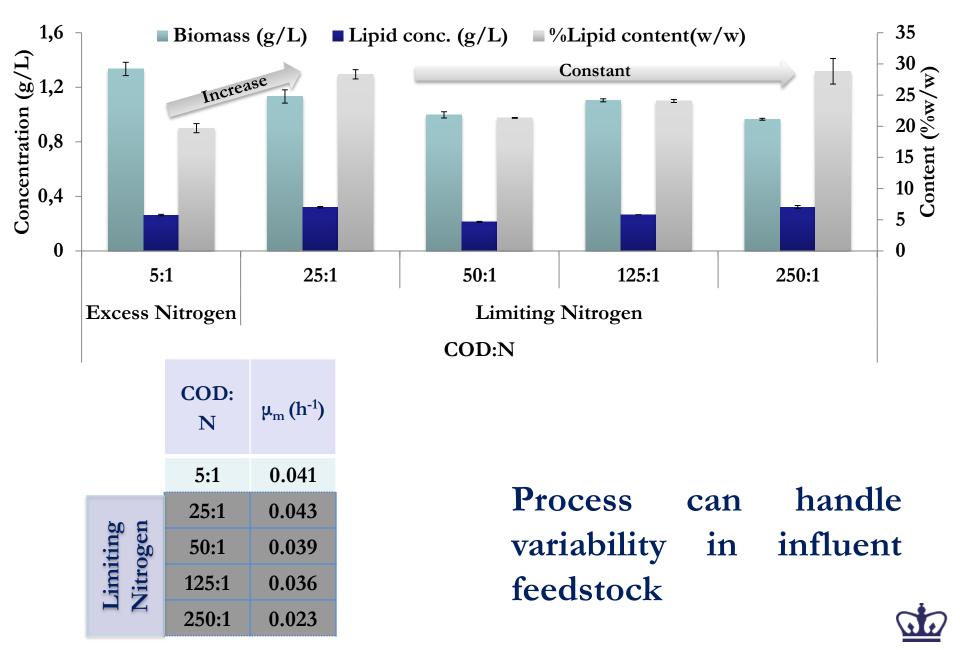
- Different initial N concentrations
 - Excess N: COD:N = 5:1
 - Limiting N: COD:N = 25:1, 50:1, 125:1, 250:1
 - StoichiometricCOD:N supply =33:1



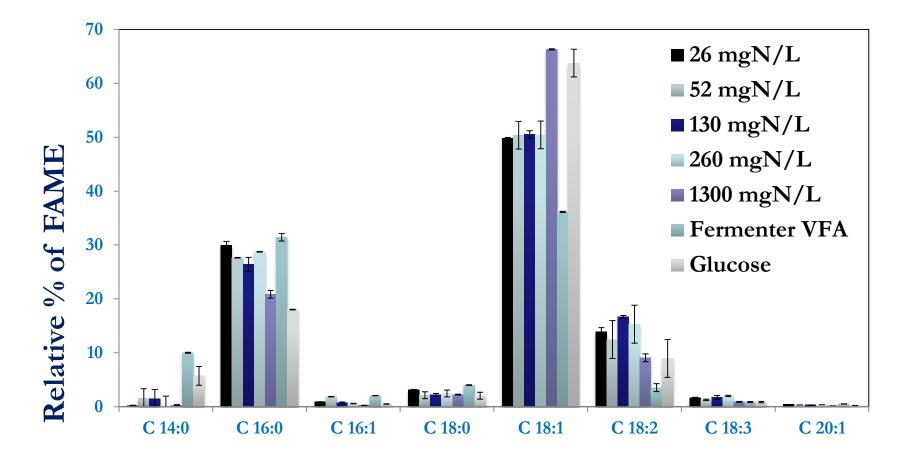
Chemostat



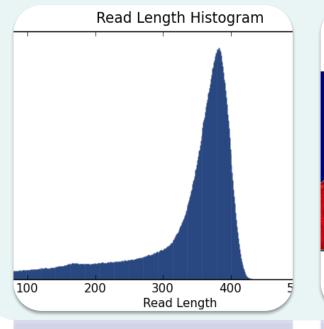
Effect of feedstock composition

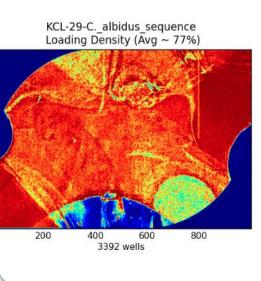


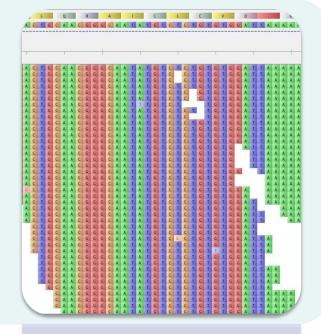
Lipid Composition



Major fatty acids accumulated are palmitic (C16:0), oleic (C18:1), and linoleic acid (C18:2) Similar to soybean oil and jatropha oil, which are used as feedstock for biodiesel production in the US and the EU







Genome of *C. albidus* sequenced. 3million reads, 1G bases, 30x genome coverage Assembly of library reads in to contiguous sequences (contigs). Consensus length 25MB, 915 contigs, N50= 83 kB Allows understanding of mechanisms and metabolic pathways for lipid accumulation.

Can be used to increase lipid accumulation even further



Economic analysis

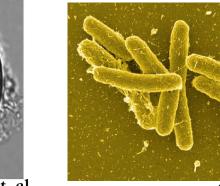
Cost of biodiesel production

Carbon source cost	\$30/ton			
	(Much lower if sludge comes in pre-fermented, as in			
	Kumasi, GH)			
Lipid yield from <i>C. albidus</i>	40.96			
(kg lipid/ton VFA)	(lowest observed value during our studies)			
Lipid cost (\$/lb)	0.33			
Gross cost (\$/L biodiesel)	0.71			
Gross cost (\$/Kg biodiesel)	0.81			

Not competing with biodiesel industry, rather making sanitation enterprise energy neutral or energy positive

Microbial inactivation using VFA

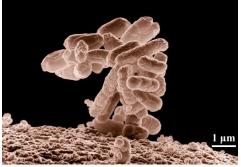




Butkus et. al

Salsali et al

Salsali et. al



Wagner et. al

Ascaris sp.

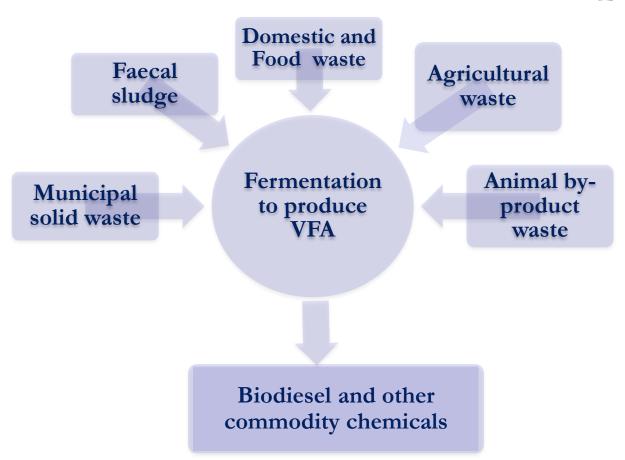
Salmonella sp.

E. coli

High VFA conc.(60 g/L) Low pH (4.75) High temperature(49°C) Low pH (5.5) High temperature(55°C) Reduction after 7 days

What is the impact of exposure to VFA under extant conditions of anaerobic fermentation?

Conclusions and implications



Novel and flexible platform to convert a variety of organic 'waste' streams to biodiesel or other lipid based commodity chemicals

Not reliant upon inherent lipid content- other organic classes can be converted to lipids

• For biodiesel as the preferred end point, reliance upon agricultural outputs is reduced or eliminated

- Links sanitation practice with energy and chemical recovery
- Microbial inactivation needs to be further characterized



DISCUSSION

BILL& MELINDA GATES foundation



Contact information Kartik Chandran Columbia University E-mail: kc2288@columbia.edu Phone: (212) 854 9027 www.columbia.edu/~kc2288/



Microbial inactivation using VFA

Different concentrations 0, 30, 300, 1000, 3000 mg/L Physical conditions from pilot plant pH 8.0, Temp 25C

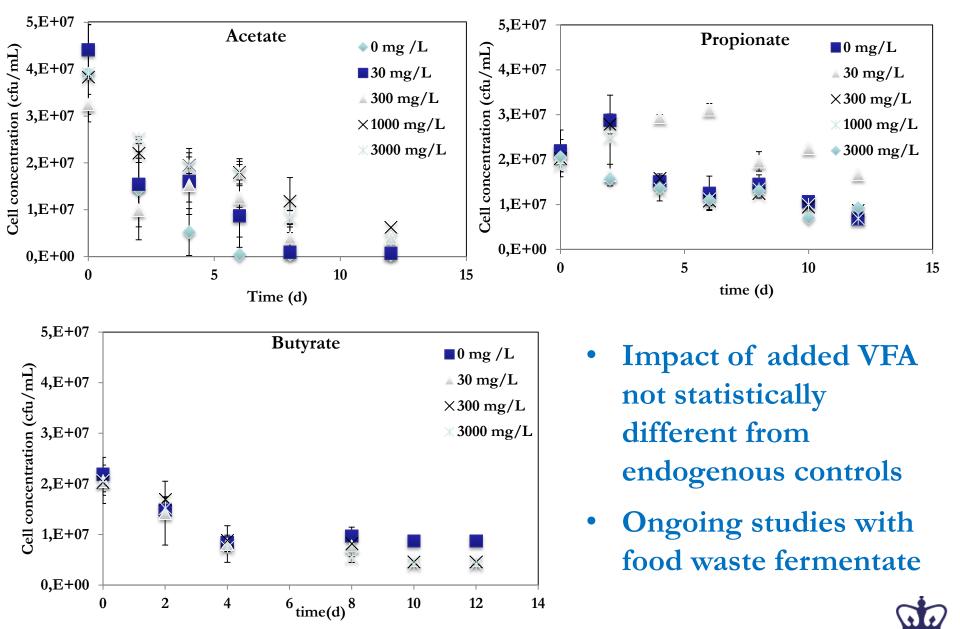
Different VFA sources

Synthetic: Acetate, Propionate, Butyrate

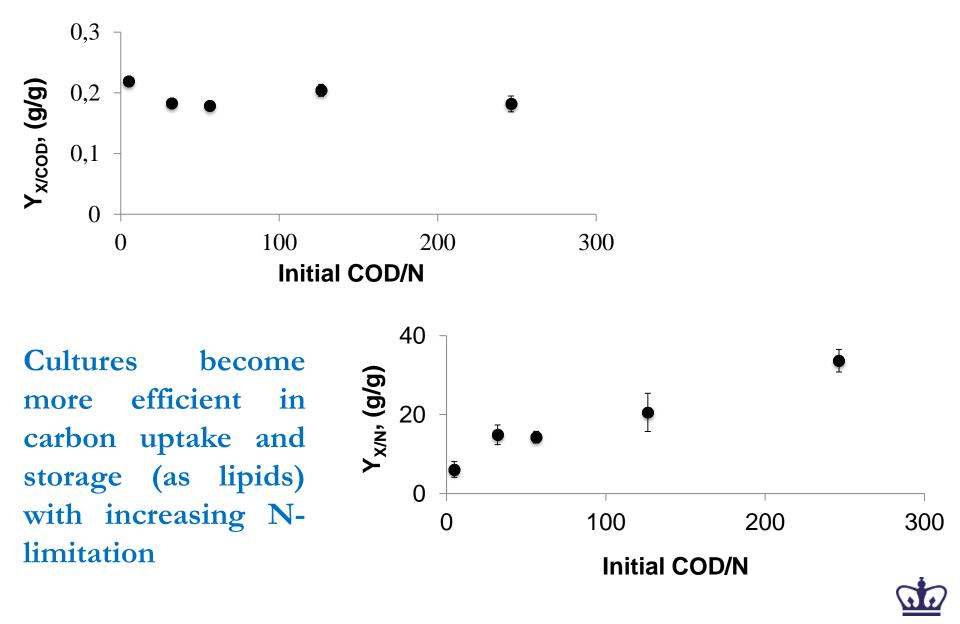
Mixed Acids from anaerobic fermenter Effect on cell viability of *E. coli* (cfu/mL) Incubation time 12 days; reflective of pilot plant in the field



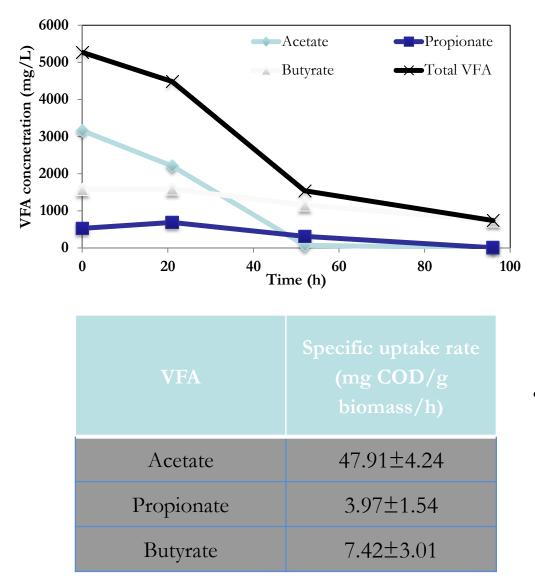
EFFECT OF SYNTHETIC VFA



EFFECT OF NITROGEN CONCENTRATION ON YIELD COEFFICIENTS



PREFERENTIAL CONVERSION OF VFA TO LIPIDS

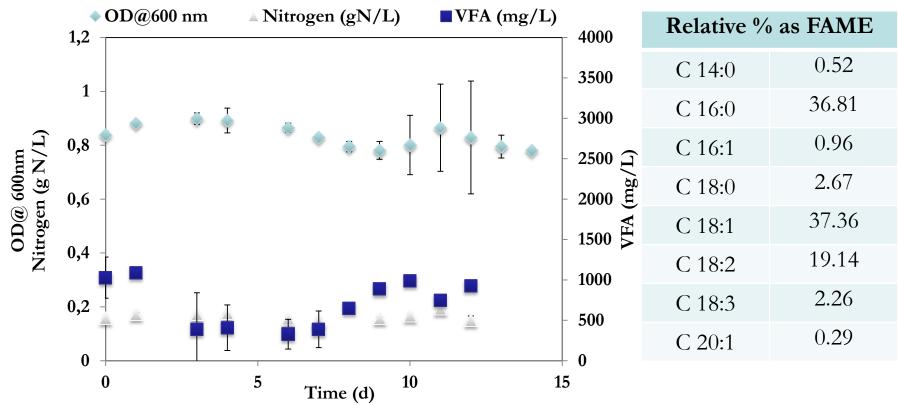


C. albidus exhibited higher preference for acetic acid before other VFAs *i.e.* propionic and butyric acid.

Specific uptake rate for acetate was higher than other VFA



BIOMASS AND LIPID YIELD IN CHEMOSTAT



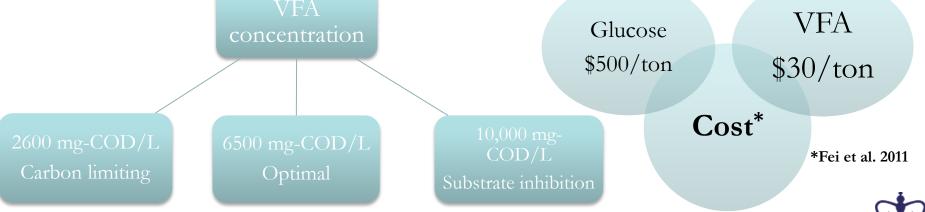
• The steady state biomass concentration was 1.02 g/L and the intracellular lipid content increased to 29.88%.

- At this operational HRT of 3 days, the cells were able to assimilate all the influent carbon source.
- Slow growth rate resulted in increase in the saturated fatty acid content.

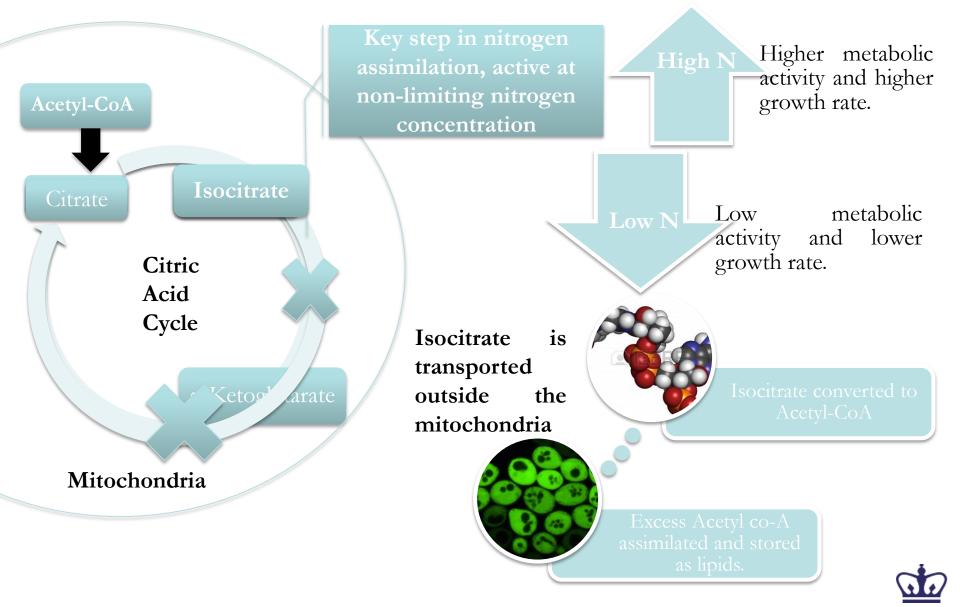


EFFECT OF DIFFERENT CARBON SOURCES AND CONCENTRATIONS

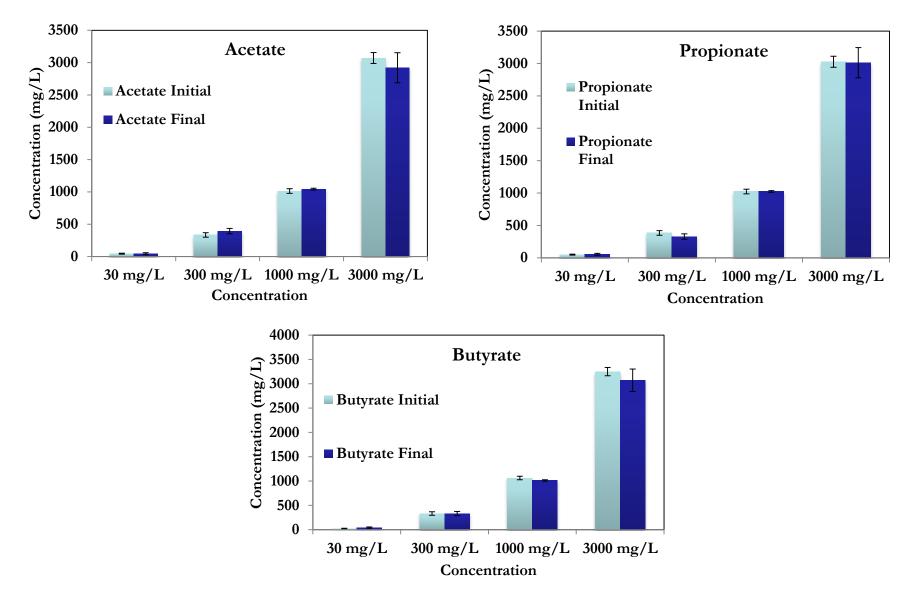
Carbon source	NH ₃ -N (mg/L)	Biomass (g/L)	μm (h ⁻¹)	Lipid content	Y _{L/ΔCOD} (mg/g)
Pure VFA	260	1.13	0.043	27.8%	52
VFA from fermenter	260	0.96	0.021	14.9%	31
Glucose	1300	5.14	0.095	43.3%	110



METABOLIC EFFECT OF NITROGEN CONCENTRATION



VFA consumption by *E. coli*





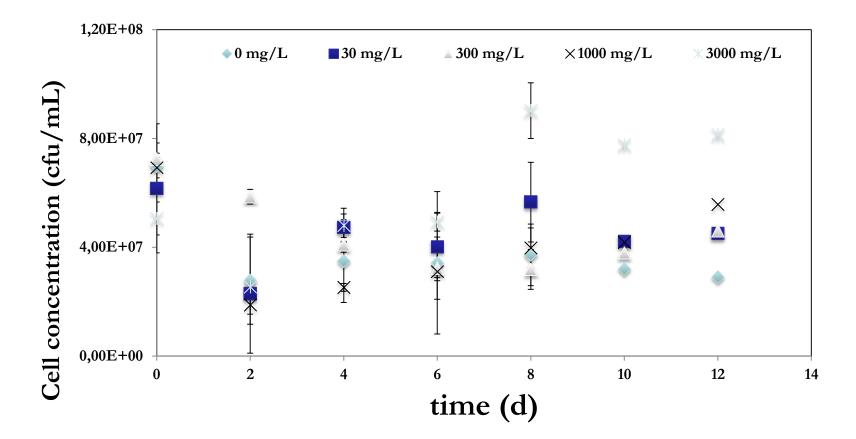
Water Chemistry

Acetate	4.75	1.78E+03
Propionate	4.88	1.32E+03
Butyrate	4.82	1.51E+03

At pH 8.0, >99.9% VFA exist as their conjugate base



EFFECT OF VFA FROM ANAEROBIC FERMENTATION OF FOOD WASTE



Impact of added VFA not statistically different from controls Additional testing ongoing

