



## **Decentralised treatment of high strength sewage in UASB and Anaerobic-Hybrid septic tanks**

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# Presentation Outline

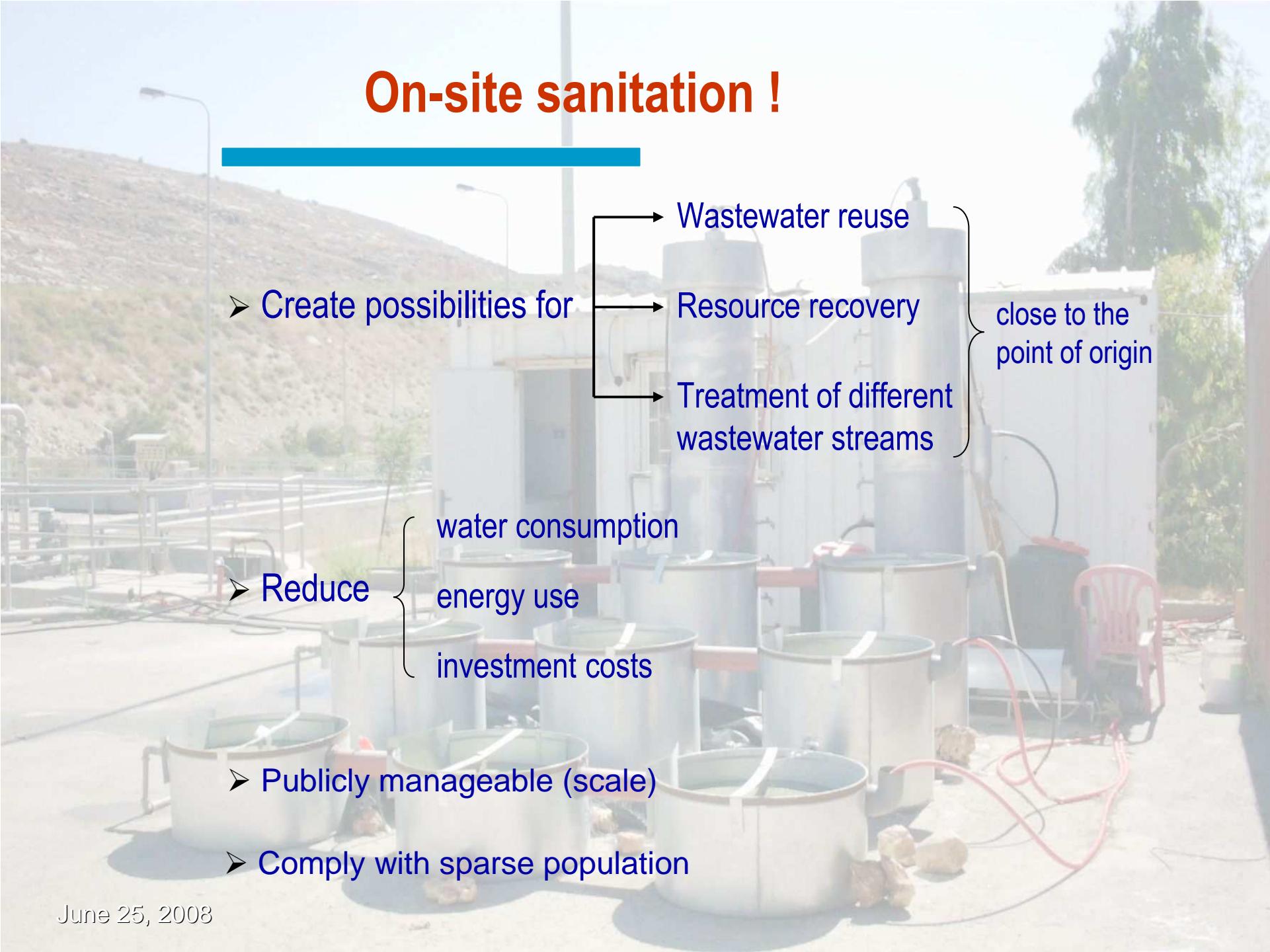
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- Background
  - Research objectives
  - Experimental set-up
  - Results
  - Conclusions & Recommendations
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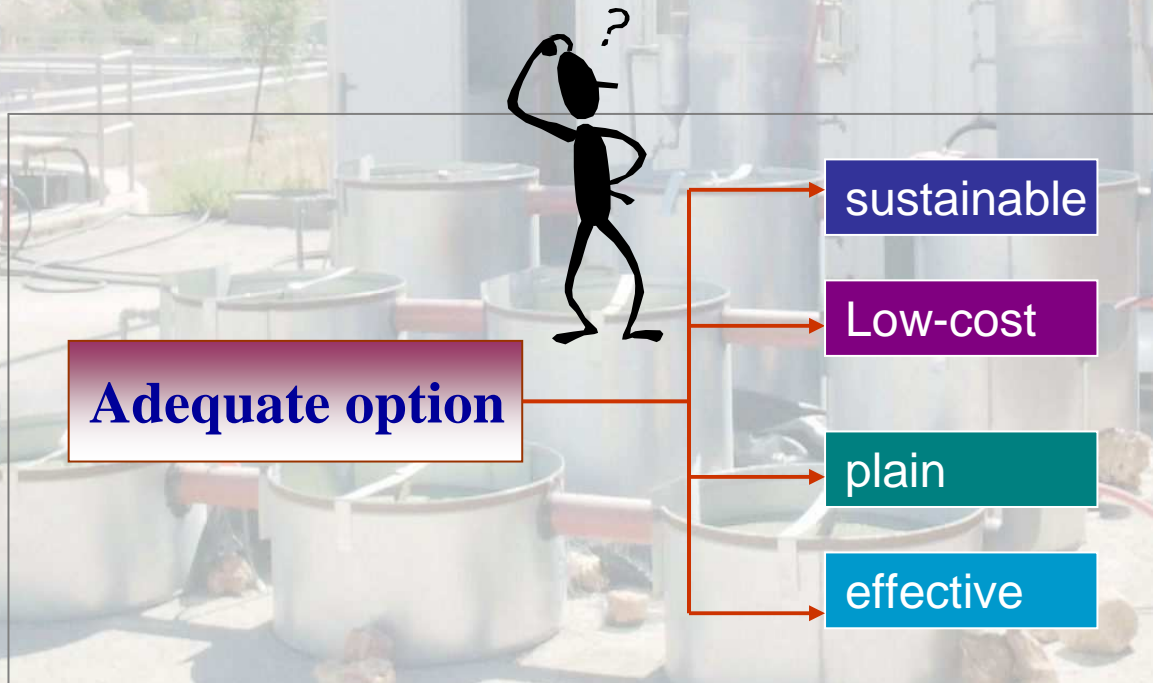
# On-site sanitation !

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- The image shows an outdoor on-site sanitation system. It consists of several large, cylindrical metal tanks arranged in a row, connected by pipes. In the foreground, there are several smaller, similar tanks. A red plastic chair is visible on the right side. The background shows a dry, hilly landscape under a clear sky.
- Create possibilities for
    - Wastewater reuse
    - Resource recovery
    - Treatment of different wastewater streams

close to the point of origin
  - Reduce
    - water consumption
    - energy use
    - investment costs
  - Publicly manageable (scale)
  - Comply with sparse population

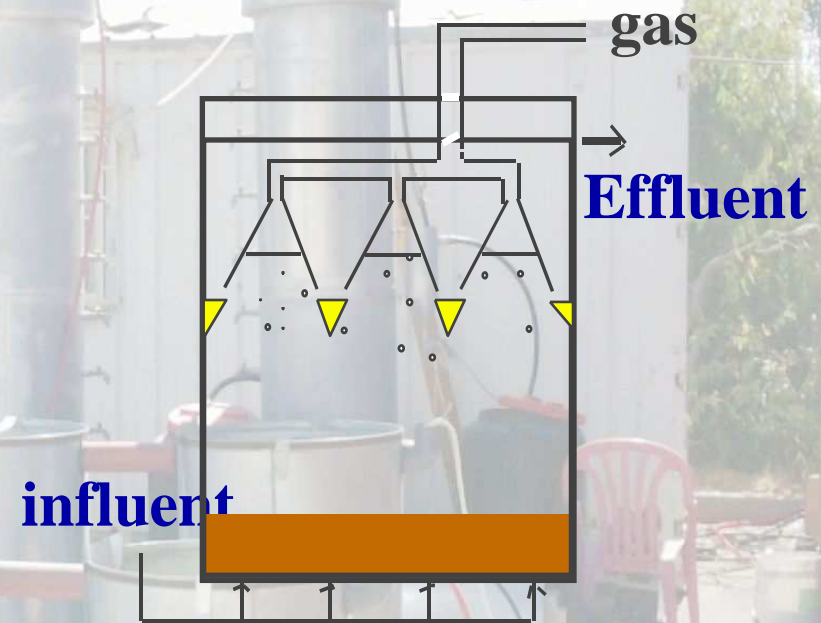
# On-site sanitation in Palestine !?

- ◆ Cesspits and septic tanks are the primary modes of on-site wastewater disposal and sewage pre-treatment.
- ◆ A sanitation intervention is needed.



✓ The UASB-septic tank system represents an effective and low-cost onsite pre-treatment alternative for domestic wastewater (Bogte *et al.*, 1993; Lettinga *et al.*, 1993).

✓ The performance of the UASB-septic tank has been recently investigated under Palestine conditions (Al-Shayah and Mahmoud, 2008; Al-Jamal and Mahmoud, 2008).



# Reactors' performance

## COD: hot period results

Parameter	UASB-septic tank 1 (R1) (HRT = 2 days)		UASB-septic tank 2 (R2) (HRT = 4 days)	
	Effluent (mg/L)	Removal (%)	Effluent (mg/L)	Removal (%)
<b>Total</b>	537 (60)	54 (6)*	493 (95)	58 (7)*
<b>Suspended</b>	97 (43)	85 (6)*	69 (29)	89 (4)*
<b>Colloidal</b>	129 (30)	27 (19)	121 (31)	32 (17)
<b>Dissolved</b>	311 (64)	12 (20)	304 (80)	14 (25)

\*: Significant difference ( $\rho < 0.05$ )

## COD: cold period results

Parameter	UASB-septic tank 1 (R1) (HRT = 2 days)		UASB-septic tank 2 (R2) (HRT = 4 days)	
	Effluent (mg/L)	Removal (%)	Effluent (mg/L)	Removal (%)
<b>Total</b>	433 (109)	51 (9)	408 (109)	54 (11)
<b>Suspended</b>	62 (34)	83 (10)*	45 (30)	87 (8)*
<b>Colloidal</b>	104 (46)	20 (32)	112 (41)	10 (37)
<b>Dissolved</b>	265 (96)	24 (15)	248 (94)	28 (18)

## Problem

✓ The achieved values of VFA and CODdis, in the system operated by Al-Shayah and Mahmoud, of 160 and 304 mgCOD/l; and the effluent biodegradable COD of 225 and 192 mg COD/l indicate that the reactor can achieve further treatment.

## Hypothesis

- ✓ The reactor performance might be improved by:
- enhancement of sludge bed methanogenic activity by for instance inoculating the reactor with well adopted sludge might further
  - provision of packing material in the upper part of the reactor

# Objectives

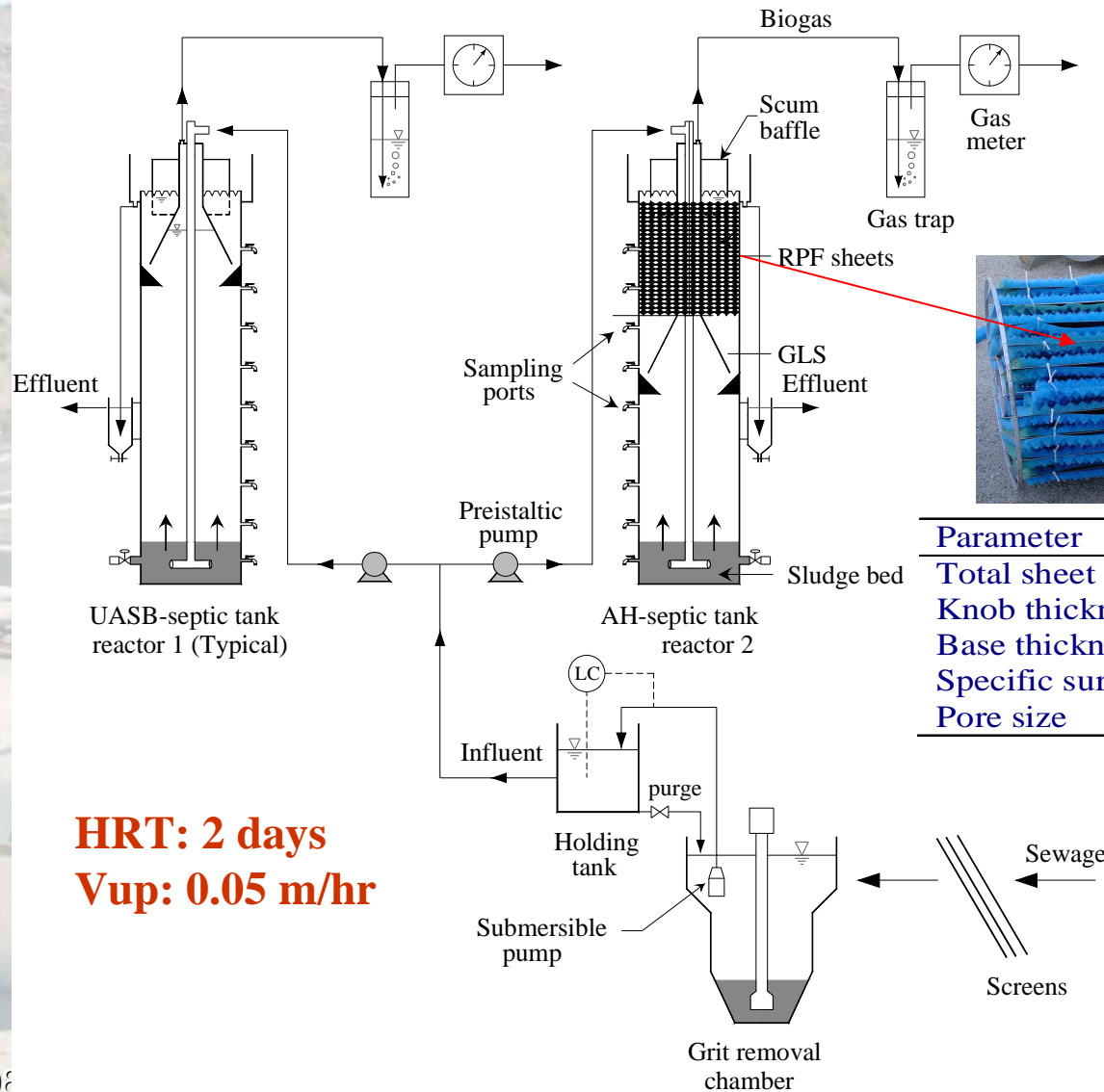
To promote a viable and affordable on-site sanitation alternative for rural communities.

## Specific objectives

- The main goal of this research is to assess the possibility of enhancing the process performance of the UASB-septic tank treating sewage under Palestinian conditions by (1) adding a packing media to the top of the reactor, thus converting the UASB-septic tank to an anaerobic hybrid-septic tank; and (2) by inoculating the reactors with sludge of good quality, viz. well adopted sludge.



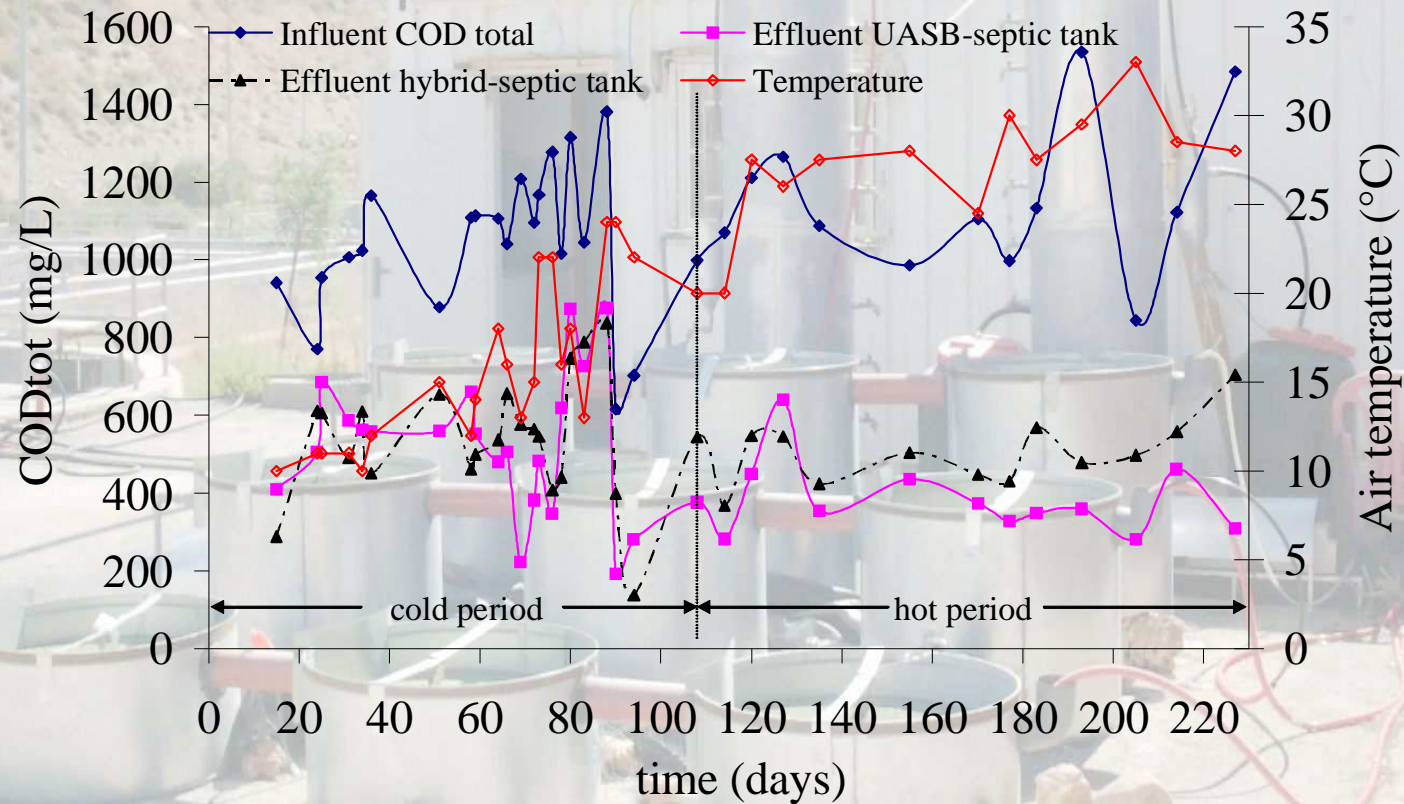
# UASB & AH-STs pilot plants



**HRT: 2 days**  
**Vup: 0.05 m/hr**

# Reactors' performance

## R1: COD Total



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# Reactors' performance

Influent and effluent COD<sub>tot</sub> and removal efficiencies (%) in a UASB-septic tank and an AH-septic tank reactors

		Cold period 15 – 108 day n = 22			Hot period 108 – 227 day n = 13		
		Influent	UASB-ST	AH-ST	Influent	UASB-ST	AH-ST
<b>COD<sub>tot</sub> (mg/l)</b>	Average	1042	520	539	1141	385	509
<b>COD removal (%)</b>	Average		50	48		66	55
<b>T<sub>air</sub> (°C)</b>	Average	16			27		

# Reactors' performance

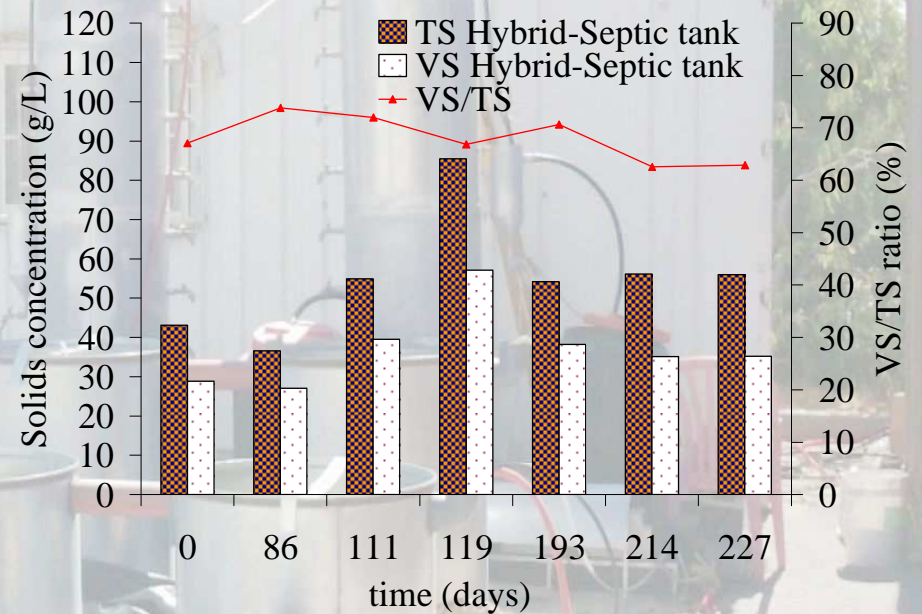
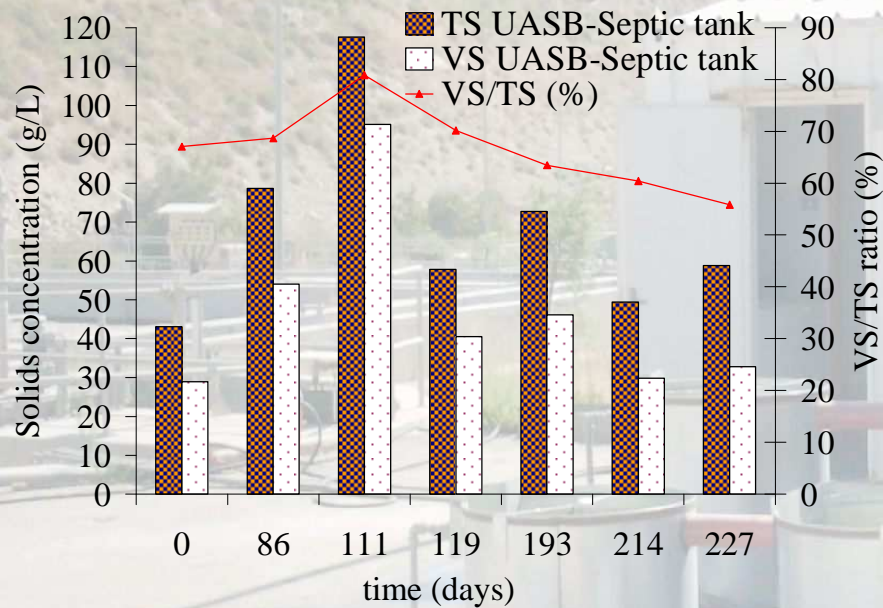
Influent and effluent conc. and removal (%) in UASB-st and AH-st

Parameter	UASB-st (HRT = 2 days)			AH-st (HRT = 2 days)	
	Influent Conc.	Effl. Conc.	R. effic. (%)	Effl. Conc.	R. effic. (%)
		AVR		AVR	
<b>COD Total</b>	1186	348	70	540	53
<b>Sus</b>	767	209	72	339	54
<b>Col</b>	111	18	77	22	78
<b>Dis</b>	308	121	55	179	45
<b>VFA as COD</b>	110	15	88	21	82
<b>NH<sub>4</sub><sup>+</sup> as N</b>	84	80	-0.06	83	1.2
<b>PO<sub>4</sub><sup>3-</sup> as P</b>	14.3	12	14	11	24
<b>TSS</b>	1125	45	94	59	95
<b>FC</b>			99.33		
	8.40E+09	3.37E+07		3.80E+07	99.16
<b>Tair (°C)</b>	29				
<b>Patm.</b>	0.92				

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Measurements over 50 days (177-227 day)

# Reactors' performance



Sludge bed development in a UASB-st and AH-st

# Reactors' performance

VS, TS, and VS/TS ratios (0-227 days)

	VS	TS	VS/TS
UASB-st	47	68	67
AH-st	37	55	68

# Reactors' performance

The VFA/CODdis had remarkably reduced from 40% in the influent to 12% in the effluent of both reactors, with a substantial decrease of VFA concentration in the effluent.

Conversion in UASB –septic tanks: 2 days HRT

Parameter	This research	Al-Shayah and Mahmoud (2008)
<b>H</b> (%)	29	16
<b>A</b> (%)	30	19
<b>M</b> (%)	36	15

# Conclusions

- ❑ The performance of the UASB-septic tank reactor was substantially improved by starting up the reactor with well adopted anaerobic sludge.
- ❑ The UASB-septic tank reactor is more efficient as compared to the AH-septic tank reactor.

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# Recommendations

- ❑ Application of UASB-septic tank for grey water treatment should be assessed.
- ❑ Application of decentralized "community onsite and/or one house or cluster on-site" in Palestine is recommended
- ❑ Performance of the reactors during the second year of operation should be assessed.
- ❑ A post-treatment step is recommended in most cases after UASB- septic tank systems.
- ❑ Hydrodynamic behavior of the UASB septic tank should be assessed



***Thank You !***

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